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MEMORANDUM

WATER-FILM COOLING OF AN 80° TOTAL-ANGLE CONE AT

A MACH NUMBER OF 2 FOR AIRSTREAM TOTAL

TEMPERATURES UP TO 3,000° R

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NATIONAL AERONAUTICS AND SPACE ADMINISTRATION

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SUMMARY

Film-cooling tests, with water as the coolant, were made on an $80^{\rm O}$ total-angle cone in a Mach number 2 free jet at sea-level pressure. The tests were made at free-stream total temperatures from 1,500° to 3,000° R and at free-stream Reynolds numbers per foot from 8×10^6 to 3×10^6 .

The tests showed that the downstream end of the model became very hot if the coolant rate was too small to cover the complete model with a water film. This water film was fairly symmetrical when the model was at zero angle of attack but was very asymmetrical when the model was at an angle of attack of 5° . A comparison with results of a previous transpiration-cooling test showed that, with water as the coolant, transpiration cooling was at least 2.5 times as efficient as the film cooling of the present tests.

INTRODUCTION

The survival of a long-range ballistic missile during atmospheric reentry depends to a great extent upon alleviating the heating load to the nose region. (See refs. 1, 2, and 3.) It has been determined from previous work that for large weight-drag ratios the problem cannot be solved by geometric considerations alone, such as blunting the nose or redistributing the material in the nose to improve the absorption of the incoming heat. Hence, many different cooling schemes have been suggested for keeping the nose of the reentry missile at a temperature that present materials can withstand. At present, however, the data available on the different cooling schemes are insufficient for direct

application to a given missile nose without some preliminary tests in which the actual proposed missile-nose shape and cooling scheme are used.

A program was initiated by the Pilotless Aircraft Research Division of the Langley Aeronautical Laboratory to determine the feasibility of using a film-cooling scheme on a proposed nose shape of a current missile. The proposed nose shape was an 80° total-angle cone and the coolant was distilled water ejected at the apex of the cone. The local airstream swept this water back over the surface of the cone in the form of a water film.

The parameters which varied in this present investigation were free-stream total temperature, angle of attack, coolant flow rate, and geometry of coolant ejection nozzle. The tests were made in the ethylene-heated high-temperature jet of the Langley Pilotless Aircraft Research Station at Wallops Island, Va. All tests were made in this 12-inch-diameter jet at sea-level pressure for a Mach number of 2.03. The values of free-stream total temperature for the tests were approximately 1,500°, 2,000°, 2,500°, and 3,000° R. Axial-type coolant nozzles of three different diameters and one umbrella-type coolant nozzle were used in the tests. The free-stream Reynolds number per foot varied during the testing program from 3×10^6 to 8×10^6 .

SYMBOLS

| Α | area, sq ft |
|---------------------------|---|
| α | angle of attack, deg |
| h | aerodynamic heat-transfer coefficient, Btu/(sec)(sq ft)(OR) |
| p | pressure, lb/sq ft |
| \mathfrak{q}_{l} | local heat-transfer rate, Btu/(sec)(sq ft) |
| Q_{A} | actual no-coolant heat load, Btu/sec |
| $\mathtt{Q}_{\mathbf{T}}$ | theoretical no-coolant heat load, Btu/sec |
| r | radius, ft |
| ρ | density of gas flow, lb/cu ft |
| S | distance along cone surface meridian from apex, ft |

T temperature, OR

V velocity of gas flow, ft/sec

weight of coolant per unit area of model, lb/sec per sq ft of model wetted area

M Mach number

Subscripts:

aw adiabatic wall

c coolant

∞ free stream

l local

t total

w wall

APPARATUS

Model

The model, shown in figure 1, was an 80° total-angle cone with a base diameter of 5.75 inches which was fabricated from type 347 stainless steel. The wall thickness of the cone was 0.050 inch. A tube was installed along the axis of the cone, terminating at the apex where coolant flow nozzles of various size and geometry could be inserted.

Drawings of the coolant nozzles are shown in figure 2. Three of the nozzles had straight through holes with inside diameters of 0.050, 0.150, and 0.200 inch. An umbrella nozzle designed to direct the flow tangentially over the body was also used. All nozzles were made of stainless steel and had external screw threads for mounting in the nose of the cone.

The locations of the thermocouples and pressure orifices are shown in figure 1. There were 20 chromel-alumel thermocouples installed on the inner surface of the cone along the two meridians in the pitch plane. Ten thermocouples were also installed on the inner surface at station 1.70 so that a thermocouple was located every 30° around the body. The water

temperature was measured with a copper-constantan thermocouple located in the coolant flow pipe at approximately the location shown on the drawing.

Seven pressure orifices were installed along the two meridians at right angles to the thermocouple meridians. One additional orifice was located on one of the thermocouple meridians. The locations of these eight orifices are shown in figure 1. All pressure tubes were soldered to the stainless-steel model with a silver solder that has a melting point of $1,175^{\circ}$ F.

Test Facility

The tests were made in a 12-inch-diameter ethylene-heated hightemperature jet of the Langley Pilotless Aircraft Research Station at Wallops Island, Va. This jet is a blowdown-type system consisting of storage spheres, a preheater, combustion chamber, and test nozzles. Air is kept in the storage spheres at a pressure of about 200 pounds per square inch and a dewpoint temperature of about -40° F. During operation, air from the spheres is preheated to approximately 9000 R and passed through ducts into a combustion chamber where ethylene is injected into the airstream. Ignition is obtained by firing a small solid-propellant rocket into the ethylene-air mixture. The products of the resulting combustion are passed through the 12-inch-diameter nozzle and exhausted at ambient sea-level pressure to obtain shock-free flow at a Mach number of 2.03. The temperature of the exhaust gas is varied by changing the ethylene-air ratio, and the static pressure of the exhaust gas is regulated with a valve upstream of the combustion chamber. The physical characteristics of this jet are discussed more fully in reference 4.

Figure 3 shows the model, with the umbrella nozzle, mounted in the jet. The upstream tip of the model was approximately 1.5 inches downstream of the exit plane of the jet nozzle, and the axes of the model and this nozzle coincided. The model was mounted on an elbow-shaped stand which encased all the thermocouple wires and pressure tubes to protect them from the high-temperature free stream. This elbow-shaped stand was mounted on a hydraulically operated, pivoted model support which provided for swinging the model into the test section after equilibrium conditions were reached. At the completion of each test the model was swung out of the jet before shutdown. Thus, the model was not subjected to the transient flow conditions which occur during the starting and shutdown of the jet.

TESTS

All tests were made in the free jet at M=2.03 with approximately sea-level static pressure conditions at the jet exit and at nominal free-stream total temperatures of 1,500°, 2,000°, 2,500°, and 3,000° R. The basic data for all tests are given in table I. The variation of temperature during each test was not more than $\pm 50^{\circ}$ R, which was considered acceptable. The free-stream Reynolds number per foot varied from 8×10^{6} at a free-stream temperature of about 1,500° R to 3×10^{6} at a free-stream temperature of about 3,000° R.

At approximately 1,500° R, a test was made with each coolant flow nozzle. The clearance between the umbrella nozzle and the model surface was 0.0025 inch. No significant differences in cooling were noted between any of these tests at 1,500° R, regardless of coolant-nozzle geometry. Hence, at 2,000° R, only the 0.150-inch-diameter axial nozzle and the umbrella nozzle (0.0025-inch clearance) were used. Also, at 2,000° R no significant differences in cooling were noted between the two types of nozzles. Hence, at 2,500° R and at 3,000° R only the 0.150-inch-diameter axial nozzle was used. To provide a basis for evaluating the effectiveness of these film-cooling tests, a test was performed without coolant at an arbitrarily chosen temperature of 1,500° R. Also, to determine the effect of angle of attack on the flow symmetry, a test was made at 1,500° R with each of the two types of coolant ejection nozzles at an angle of attack of 5°.

At the beginning of each test, the model was held out of the jet until the free-stream flow became steady. Then the coolant flow was started at a high rate and the model was swung into the jet. It took approximately I second for the model to reach the center line of the jet. When the model reached the center line, a microswitch on the arm of the injector stand made contact and the resulting signal was indicated on the recorder. The test then continued at sea-level free-stream pressure for approximately 40 seconds. During this time the coolant flow rate was reduced in steps until the downstream end of the model got hot. Then the coolant flow rate was increased in steps until approximately the original flow rate was obtained. No attempt was made to obtain identical decreasing and increasing stepwise flow rates.

RESULTS AND DISCUSSION

Pressure Distributions

A typical pressure distribution for each of the two different types of coolant flow nozzles is shown in figure 4. In these plots the local

surface pressure on the cone is expressed as a fraction of the free-stream stagnation pressure and plotted against model station. The data in this figure are for tests B-1807 (using a 0.150-inch-diameter axial coolant nozzle) and for B-1808 (using the umbrella coolant nozzle). The two identical symbols at each station represent the pressures for the two orifices at each station. Since there were no significant differences in the pressures on opposite meridians of the model, the angle of attack was apparently very close to zero.

The pressure distributions in figure 4 agree closely with those for all the other tests at zero angle of attack. The pressure distributions were apparently unaffected by changes in the diameter of axial coolant nozzles, in free-stream total temperature, and in coolant flow rate. Different types of nozzles, however, caused differences in the pressure distributions. The pressures near the tip of the cone were considerably less with the umbrella nozzle than with the axial flow nozzles. The tip geometry of the model was different for these two types of coolant nozzles. Apparently the local airstream on the forward part of the model expanded more when the umbrella nozzle was used, causing the low-pressure region shown in figure 4.

The pressure distribution predicted by cone theory (assuming a sharp tip) is also shown in figure 4. The pressures from both tests approach the theoretical pressure at the downstream end. Evidently the blunt tip of each nozzle forced the cone shock to be detached and hence caused the pressures over the whole model surface to be less than the theoretical pressures.

Temperature Distributions

Shown in figure 5 is the temperature distribution for a series of coolant rates for a typical test (B-1807). The temperatures are presented in the form of the parameter $T_{\rm W}$ - $T_{\rm C}/T_{\rm aW}$ - $T_{\rm C}$ where $T_{\rm W}$ is the equilibrium temperature of the cooled wall, $T_{\rm aW}$ is the theoretical equilibrium temperature of the uncooled wall, and $T_{\rm C}$ is the original temperature of the water.

The data for each test were obtained by decreasing the coolant flow rate in steps until the model became hot on the downstream end and then increasing it in steps to approximately the original rate. The method of plotting used in figure 5 depicts the approximate temperature distribution on the model surface for each coolant flow rate and assisted in the fairing of the data toward a family of curves.

The model was constructed to allow temperatures to be obtained on opposite meridians. In addition, several temperature measurements were

to be obtained at the 1.70-inch station on other meridians. In general, all the temperatures at the 1.70-inch station were in good agreement. Hence, to simplify the plot, only the temperatures on the two primary temperature-measuring meridians are plotted in figure 5. Some of the thermocouples were inoperative during the tests, and thus a complete temperature distribution on each of the two meridians could not be obtained. The temperatures that could be plotted are shown in the figure. Double symbols for a given station represent the temperatures on the two opposite meridians of the model. The agreement for most stations was good.

Figure 5 indicates that the water film for the four highest coolant flow rates extended completely to the measuring station farthest downstream; however, for the four lower coolant flow rates, the water film did not extend that far. For these lower coolant flow rates, a thermocouple on one side of the model would sometimes be covered with a water film while that on the opposite side at the same station would not. This fact indicated an asymmetry which appeared from the temperature distributions to be small in area. This slight asymmetry of the water film helped in some cases to locate more closely the downstream extent of the water film. The basic temperature data are given in table I.

Temperature and Coolant-Rate Parameters

A composite plot of temperature parameter against coolant-rate parameter is shown in figure 6 for all tests at zero angle of attack. The temperature parameter in this figure is for the thermocouple station farthest downstream, where the maximum temperatures always occurred. A similar plot of this type could be made for any other station on the model; however, the point of maximum temperature will be of greatest interest to the designer of a cooling system.

As the free-stream total temperature was increased the data, as shown in figure 6, became more sparse. This made the fairing of the higher temperature data somewhat in doubt. However, since the fairing of the 1,500° R data was fairly well established, the data at other temperatures were faired with a similar curve. At a free-stream total temperature of 3,000° R, no recorded data were obtained for coolant flow rates low enough to cause the model to become hotter than the boiling point. For this test, the break in the temperature curve was made at the lowest flow rate. A visual indicator used for monitoring revealed, during this 3,000° R test, that the downstream thermocouple station (thermocouple 1) was becoming hot at this low flow rate. The operator did not reduce the flow rate further for fear that the model would become hot enough to melt out the silver solder holding the pressure tubes in place. Therefore, from visual data that are not presented

in this figure, it is believed that the fairing of the data for $3,000^{\circ}$ R is approximately correct.

As indicated on figure 6, four different coolant nozzles were used in the tests at 1,500° R and two at 2,000° R. There were no significant differences in the results due to differences in the coolant nozzles.

The dashed curve which represents the locus of boiling points on the figure was calculated for each of the free-stream total temperatures. This was done by calculating the value of $T_{\rm w}$ - $T_{\rm c}/T_{\rm aw}$ - $T_{\rm c}$ for boiling at each free-stream total temperature and then fairing the dashed curve so that it would pass through the solid $T_{\rm t,\infty}$ curves at the respective boiling point values. For values of the flow parameter between 0 and 0.0014, the curve was faired from a knowledge of the two end points and the approximate point at 1,000° R. The value of $T_{\rm w}$ - $T_{\rm c}/T_{\rm aw}$ - $T_{\rm c}$ for boiling was calculated for 1,000° R as for the other $T_{\rm t,\infty}$. At a $T_{\rm t,\infty}$ value of 1,000° R, the value of flow-rate parameter was obtained by a cross fairing of $T_{\rm t,\infty}$ against flow-rate parameter as shown in figure 7.

Figure 7 presents the minimum flow rates necessary to maintain the water film to the thermocouple station farthest downstream at different free-stream total temperatures. For free-stream temperatures above 1,500° R, this curve apparently is a straight-line function of the free-stream total temperature. Below 1,500° R, the curve was faired to the calculated end point at a flow-rate parameter of zero. The minimum flow rate necessary to cool the entire model at $T_{\rm t,\infty}=1,000^{\circ}$ R is seen from this curve to be 0.0003. This is the value of flow-rate parameter at which the boiling point was plotted in figure 6 for $T_{\rm t,\infty}=1,000^{\circ}$ R.

As mentioned previously, the data in figure 6 are all for the thermocouple station farthest downstream. When the water rate is just sufficient to cover the model with a film back to this point, the temperature parameter at this station is seen to correlate very well with the boiling-point curve. The data of reference 5 for the station at the downstream end of the water film are shown in figure 6 by a solid symbol which also correlates with this boiling-point curve.

If the data are correlated on the basis of average surface temperature, different results will be obtained. At low heating rates such as existed in the tests of reference 5 ($T_{t,\infty}=1,000^{\circ}$ R), the average temperature correlates very closely with the saturated vapor temperature. At high heating rates such as existed in the present tests at $T_{t,\infty}=3,000^{\circ}$ R, the average temperature correlates better with the boiling temperature.

Efficiency of Film Cooling

The primary purpose of making these film-cooling tests was to obtain the data shown in figure 6. However, since the present method of cooling is not the only one that is being considered for possible use in cooling reentry models, some of the data are also presented in a form that shows the effectiveness or efficiency of the film-cooling method. Also, in this form the data from other cooling methods can be compared with the film-cooling method used in the present tests.

Figure 8 presents the data in the form of an efficiency factor Q_A/Q_T plotted against coolant flow-rate parameter $W/\rho_l V_l$. As used in this report, Q_A is the actual no-coolant heat load that would have existed on the model at the wall temperature of the cooling test. It was obtained by integrating the local heat loads over the complete model surface. The local heat loads were calculated for each station from the equation

$$q_l = h_l(T_{aw,l} - T_{w,l})$$

Then the actual no-coolant total heat load was obtained from the following integration

$$Q_A = \int_A q_l dA = 2\pi \int_S q_l r_l dS$$

This value of Q_A may not be the actual value of heat that is being absorbed by the water film, since the heat-transfer coefficient and equilibrium wall temperature may have varied considerably from their values on the dry wall. Reference 6 shows how the presence of a water film varies the heat-transfer coefficient, and reference 7 shows how the presence of a coolant varies the equilibrium wall temperature. This value of Q_A is a good reference number, however, that can be readily calculated for most model shapes for a given wall temperature.

As used in this report, Q_{T} is the theoretical no-coolant heat load that could have existed on the model at the wall temperature of the cooling test, based on the assumption that the full cooling capacity of the water was used. It was obtained by calculating the total heat necessary to raise the cooling water from its entering enthalpy to its final enthalpy. It may be shown in equation form as

 $Q_T = WA(Coolant final enthalpy - Coolant entering enthalpy)$

The coolant final enthalpy was always based on the average wall temperature of the model or on the boiling temperature of water on the model, whichever was greater. Always included in \mathbf{Q}_{T} was the heat of vaporization.

Figure 8 shows that at each value of $T_{t,\infty}$ the efficiency increased as the coolant flow rate decreased. For some reason the curves all seemed to tend toward $Q_A/Q_T=0.40$. This would seem to indicate that this method of film cooling is limited in efficiency to 40 percent.

The minimum value of the flow rate parameter corresponding to complete coverage of the model with a water film was determined for each value of $T_{t,\infty}$ in the present tests and in reference 5. The locus of these points in figure 8 is the straight line at $Q_A/Q_T=0.26$. Hence, the film cooling used in these tests is approximately 26 percent efficient if the minimum value of coolant flow rate is used to maintain a water film on the complete model. If more than this flow rate is used the efficiency decreases, and if less than this flow rate is used the efficiency increases. A disadvantage of decreasing the flow rate, however, is that the downstream end of the model becomes hot.

Also shown in figure 8 are the data from reference 8 which present the results of transpiration-cooling tests on an 8° total-angle cone at $T_{t,\infty}=1,000^{\circ}$ R. At the highest three flow rates of these transpiration tests the model temperature was maintained at approximately 125° to 140° F. At the lowest flow rate the flow was unsymmetrical as a result of gravity effects and part of the model became hot. From the data as presented in reference 8, it appears that this lowest flow rate would also have cooled the model below saturated steam temperature if the gravity effects had not existed. Hence, the straight line in figure 8 at $Q_{\rm A}/Q_{\rm T}=0.65$ is only approximate and perhaps should be at an even higher value. This $Q_{\rm A}/Q_{\rm T}=0.65$ is the approximate level of efficiency for minimum flow rates necessary to keep the complete model surface below saturated steam temperature. It appears from figure 8 that the transpiration-cooling method of reference 8 was at least 2.5 times as efficient as the film cooling of the present tests.

Effect of Angle of Attack

Included in the program were two tests at $\alpha = 5^{\circ}$ to determine the effect of angle of attack on the symmetry of the water film. The basic

data from these two tests are given in table I. These tests were not originally intended to be included in the program. Hence, the model was not oriented in the jet to give the best data; that is, the main thermocouple meridians were not on the leeward and windward sides of the model but were 90° from these positions. However, motion pictures of the tests and sediment rings on the model indicated that the water film on the model surface was very asymmetrical at $\alpha = 5^{\circ}$.

Two sketches (fig. 9) depict approximately this water-film asymmetry at $\alpha=5^{\circ}$ for each type of nozzle. It was thought that the umbrella-type nozzle would be less affected by angle of attack than the axial-type nozzle. However, the motion pictures and sediment rings did not show any significant difference between the two types of nozzles. Apparently this water film starts fairly symmetrically at the tip of the cone but, as a result of boundary-layer cross flow or pressure differences, the coolant is forced from the windward side to the leeward side.

SUMMARY OF RESULTS

Film-cooling tests, with water as the coolant, were made on an 80° total-angle cone in a free jet at sea-level pressure. The Mach number of the tests was 2.03 and the free-stream total temperatures were approximately 1,500°, 2,000°, 2,500°, and 3,000° R. The following results were obtained:

- 1. As the coolant rate was progressively reduced below the minimum required to keep a water film on the complete model, the temperature at the downstream end of the model became progressively higher.
- 2. There were no significant differences between the cooling results achieved with the axial nozzle and with the umbrella nozzle.
- 3. For the minimum coolant rates necessary to cover the complete model with a water film, the efficiency for all tests was approximately 26 percent, based on the total cooling capacity of the water.
- 4. When water is used as the coolant, transpiration cooling is at least 2.5 times as efficient as the film cooling of the present tests.
- 5. The water film on the model surface was fairly symmetrical for all tests at $\alpha = 0^{\circ}$ but was very asymmetrical for all tests at $\alpha = 5^{\circ}$.

Langley Research Center,
National Aeronautics and Space Administration,
Langley Field, Va., July 17, 1958.

REFERENCES

- 1. Allen, H. Julian, and Eggers, A. J., Jr.: A Study of the Motion and Aerodynamic Heating of Missiles Entering the Earth's Atmosphere at High Supersonic Speeds. NACA TN 4047, 1957. (Supersedes NACA RM A53D28.)
- 2. Carter, Howard S., and Bressette, Walter E.: Heat-Transfer and Pressure Distribution on Six Blunt Noses at a Mach Number of 2. NACA RM L57C18, 1957.
- 3. Purser, Paul E., and Hopko, Russell N.: Exploratory Materials and Missile-Nose-Shape Tests in a 4,000° F Supersonic Air Jet. NACA RM L56J09, 1956.
- 4. English, Roland D., Spinak, Abraham, and Helton, Eldred H.: Physical Characteristics and Test Conditions of an Ethylene-Heated High-Temperature Jet. NACA TN 4182, 1958.
- 5. O'Sullivan, William J., Chauvin, Leo T., and Rumsey, Charles B.: Exploratory Investigation of Transpiration Cooling to Alleviate Aerodynamic Heating on an 80 Cone in a Free Jet at a Mach Number of 2.05. NACA RM L53H06, 1953.
- 6. Kinney, George R., Abramson, Andrew E., and Sloop, John L.: Internal-Liquid-Film-Cooling Experiments With Air-Stream Temperatures to 2,000° F in 2- and 4-Inch-Diameter Horizontal Tubes. NACA Rep. 1087, 1952. (Supersedes NACA RM E50F19 by Kinney and Sloop, NACA RM E51C13 by Kinney and Abramson, and NACA RM E52B20 by Kinney.)
- 7. Rubesin, Morris W., Pappas, Constantine C., and Okuno, Arthur F.:
 The Effect of Fluid Injection on the Compressible Turbulent
 Boundary Layer Preliminary Tests on Transpiration Cooling of a
 Flat Plate at M = 2.7 With Air As the Injected Gas. NACA
 RM A55I19, 1955.
- 8. Chauvin, Leo T., and Carter, Howard S.: Exploratory Tests of Transpiration Cooling on a Porous 8° Cone at M = 2.05 Using Nitrogen Gas, Helium Gas, and Water as the Coolants. NACA RM L55C29, 1955.

TABLE I.- BASIC DATA

(a) Test B-1805

| Coolant n | ozz] | Le | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|------------|------|-------------|--------------|-----|-----|------|-----|----------------|-----|-----|-----|-----|------------------|----|-----|-----|-----|---|---|---|---|---|---|---|---|---|---|---|---|---|-------|
| Type . | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | Axial |
| Diamete: | r, i | n. | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 0.200 |
| Temperatu | re c | f | c | oc. | Laı | nt | , (| ^o R | | | | | | | | | | | | | | | | | | | | | | | 515 |
| Total temp | pera | ιtι | \mathbf{r} | 9 (| ρſ | f | ree | 9 8 | str | e | ım. | , (| PR. | | | | | | | | | | | | | | | | | | 1,500 |
| Static pro | essi | $r\epsilon$ | . (| ρſ | f | ree | e : | sti | cea | ım. | ,] | b | $\prime_{ m sc}$ | 1 | in. | . ε | abs | 5 | | | | | | | | | | | | | 14.40 |
| Total pres | ssur | ·e | oi | f 1 | fre | ee | S | tre | an | 1, | 11 | o/ε | ps | ir | n. | al | os | | | | | | | | | | | | | | 120.4 |
| a, deg . | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 0 |
| Model sur | face | ŗ | re | ess | รนม | re , | , . | Lb, | /sc | 1 1 | ln. | . 8 | ibs | з, | at | t - | _ | | | | | | | | | | | | | - | • |
| Orifice | 1 | | | | | | | • | | | | | | | | | | | | | | | | | | | | | | | 54.6 |
| Orifice | 2 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 49.3 |
| Orifice | 3 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 50.3 |
| Orifice | 4 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 49.8 |
| Orifice | 5 | | | | : | | | | | | | | | | | | | | | | | | | | | | | | | | 51.2 |
| Orifice | 6 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 50.9 |
| Orifice | 7 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 55.3 |
| Orifice | 8 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 57.4 |
| | | | | | | | | | | | | | | | | | | | - | - | - | - | - | • | • | • | • | • | • | ٠ | 21. |

| Thermocouple | | Temperature coolant f | on cooled wa | all, ^O R, for 'sec, of - | |
|---|---|---|--|---|---|
| | 0.0875 | 0.0670 | 0.0500 | 0.0347 | 0.0194 |
| 1 2 3 | 691 710 | 690 675 | 708 710 | 1,340 | 1,330 1,300 |
| 24 56 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24 25 26 27 28 29 | 683 679 665 655 655 644 617 529 573 636 648 682 678 680 732 707 722 678 675 669 668 669 665 | 672 672 660 655 650 630 585 570 630 655 675 669 663 663 663 663 663 665 665 6667 | 672 672 672 658 655 655 593 577 648 663 664 655 665 665 665 665 6669 | 790 740 684 676 677 668 636 589 668 676 687 683 691 726 772 1,063 763 675 675 738 681 686 697 | 1,175 740 680 668 666 657 637 588 672 692 763 756 1,215 1,208 990 1,315 800 726 780 750 860 698 686 |
| 30 | 681 | 660 | 660 | 697 686 | 693 |

TABLE I.- BASIC DATA - Continued
(b) Test B-1807

| Coolant nozz | | | | | | | | | | | | | | | | | | | | | | | | | |
|--------------|-----------|-----|-----|-----|-----|-----|-----|-----|-----|------|-----|-----|-----|-----|-----|----|---|---|--|--|--|--|--|---|-------|
| Туре | | | | | | | | | | | | | | | | | | | | | | | | | Axial |
| Diameter, | | | | | | | | | | | | | | | | | | | | | | | | | 0.050 |
| Temperature | $\circ f$ | cc | ool | Laı | ıt, | , (| PR | | | • | | | | • | | | | • | | | | | | • | 515 |
| Total temper | ati | ure | e (| σf | fr | ee | 9 8 | tr | ee | ım , | , (| R | | | | | | | | | | | | | 1,460 |
| Static press | ur | e d | of | f | cee | 2 5 | str | ea | m, | , 1 | b/ | /sc | 1 1 | ln. | . 8 | bs | 3 | | | | | | | | 14.80 |
| Total pressu | re | of | f f | re | ee | st | tre | an | ٠, | 11 | /8 | q | ir | ı. | at | s | | | | | | | | | 120.4 |
| a, deg | | | | | | | | | | | | | | | | | | | | | | | | | 0 |
| Model surfac | e j | pre | 289 | su | re, | ,] | Lb/ | ′sg | _ 1 | n. | . 8 | bs | ٠, | at | ; - | - | | | | | | | | | |
| Orifice l | | | | | | | | | | | | | | | | | | | | | | | | | 54.3 |
| Orifice 2 | | | | | | | | | | | | | | | | | | | | | | | | | 51.4 |
| Orifice 3 | | | | | | | | | | | | | | | | | | | | | | | | | 51.1 |
| Orifice 4 | | | | | | | | | | | | | | | | | | | | | | | | | 50.8 |
| Orifice 5 | | | | | | | | | | | | | | | | | | | | | | | | | 53.1 |
| Orifice 6 | | | | | | | | | | | | | | | | | | | | | | | | | 52.6 |
| Orifice 7 | | | | | | | | | | | | | | | | | | | | | | | | | 55.0 |
| Orifice 8 | | | | | | | | | | | | | | | | | | | | | | | | | 57.5 |
| | | | | | | | | | | | | | | | | | | | | | | | | | |

| Thermocouple | | Te | mperatur coolant | e on coo | led wall ce, lb/se | , OR, fo | or | |
|--|--|--|--|--|--|--|--|--|
| Thermocoupte | 0.0695 | 0.0611 | 0.0514 | 0.0447 | 0.0410 | 0.0319 | 0.0285 | 0.0181 |
| 1 2 | 713 684 | 687 683 | 731 705 | 780 737 | 1,020 8 0 6 | 1,138 1,073 | 1,210 1,176 | |
| 3 4 5 6 7 8 9 | 668 664 654 656 650 636 | 668 664 654 667 662 691 | 673 668 654 661 641 685 | 679 668 699 656 656 642 | 702 668 654 667 | 690 679 660 661 661 653 | 724 685 660 661 650 653 | 923 702 670 639 662 659 |
| 10 11 12 13 14 15 16 | 585 642 656 688 667 665 | 573 652 661 703 672 661 | 568 647 661 651 667 665 | 573 642 656 688 667 665 | 573 652 667 703 679 676 | 585 656 661 696 684 700 | 577 658 661 696 686 73 ⁴ | 584 658 667 742 751 1,049 |
| 17 18 19 | 681 712 | 660 686 | 687 708 | 725 744 | 720 744 | 1,084 1,121 | 1,185 1,220 | 1,196 1,213 |
| 20 21 22 | 667 654 | 689 660 | 696 660 | 672 654 | 718 666 | 689 66 0 | 778 700 | 785 711 |
| 23 24 25 26 27 28 | 663 660 660 662 658 | 656 660 660 662 657 | 663 660 660 662 663 | 663 660 666 662 658 | 656 660 670 662 663 | 671 660 707 667 663 | 671 665 686 671 672 | 708 684 688 688 |
| 29 30 | 661 | 667 | 667 | 661 | 667 | 671 | 671 | 667 |

(c) Test B-1808

| Coolant nozzle | |
|---|-------------|
| Type | nbrella |
| Clearance, in | 0.0025 |
| Temperature of coolant, OR | 51 0 |
| Total temperature of free stream, OR | 1,460 |
| Static pressure of free stream, lb/sq in. abs | 14.80 |
| Total pressure of free stream, lb/sq in. abs | 120.4 |
| a, deg | 0 |
| Model surface pressure, lb/sq in. abs, at - | |
| Orifice 1 | 56.4 |
| Orifice 2 | 52.4 |
| Orifice 3 | 39.5 |
| Orifice 4 | 40.1 |
| Orifice 5 | 54.3 |
| Orifice 6 | 52.9 |
| Orifice 7 | 55.8 |
| Orifice 8 | 57.9 |
| | |

| Thermocouple | | | | | ed wall, | OR, for | | |
|--|--|--|--|--|--|--|--|--|
| Inclinocoup IC | 0.0535 | 0.0500 | 0.0410 | 0.0334 | 0.0299 | 0.0250 | 0.0188 | 0.0126 |
| 1 2 3 | 736 880 | 850 761 | 985 691 | 1,110 825 | 1,320 1,295 | 1,280 1,175 | 1,280 1,250 | 1,320 1,295 |
| 5 6 | 666 600 650 659 | 681 660 656 668 | 692 676 656 665 | 732 687 663 668 | 755 720 683 668 | 770 726 679 673 | 1,202 938 722 685 | 1,278 1,250 878 732 |
| 7 8 9 | - 638 | | 648 | | 661 | | | 661 |
| 10 11 12 13 14 15 16 | 562 632 642 695 665 660 | 571 645 658 704 669 666 | 567 644 653 695 665 660 | 571 655 658 704 669 666 | 575 655 653 704 665 667 | 571 660 664 704 665 666 | 576 661 658 704 668 670 | 580 655 653 704 703 742 |
| 17 18 19 20 | 667 687 | 688 736 | 683 705 | 722 763 | 716 960 | 722 753 | 1,230 1,200 | 1,210 1,260 |
| 21 22 | 686 656 | 679 | 725 724 | 679 | 1,195 701 | | | 1,305 |
| 23 24 25 26 27 28 | 665 656 656 665 666 | 669 668 668 673 674 | 726 724 724 728 729 | 669 668 672 673 674 | 666 667 667 668 669 | 669 668 672 674 680 | 675 672 679 685 690 | 668 667 679 673 711 |
| 29 30 | 666 | 672 | 726 | 672 | 720 | 1,315 | 1,315 | 720 |

TABLE I.- BASIC DATA - Continued

(d) Test B-1809

| Coolant nozzle | |
|---|----------|
| Type | Umbrella |
| Clearance, in | 0.0025 |
| Temperature of coolant, OR | 515 |
| Total temperature of free stream, OR | 2,000 |
| Static pressure of free stream, lb/sq in. abs | 14.80 |
| Total pressure of free stream, lb/sq in. abs | 120.0 |
| α, deg | 0 |
| Model surface pressure, lb/sq in. abs, at - | |
| Orifice 1 | 55.1 |
| Orifice 2 | 51.0 |
| Orifice 3 | 41.5 |
| Orifice 4 | 38.8 |
| Orifice 5 | 54.3 |
| Orifice 6 | 53.7 |
| Orifice 7 | 54.5 |
| Orifice 8 | 56.6 |

| Thermocouple | | Te | | e on coo flow rat | | | r | |
|----------------------------------|--|--|--------------------------|---------------------------------|--|--|--|--|
| incimocoupie | 0.1110 | 0.1048 | 0.1006 | 0.0945 | 0.0924 | 0.0750 | 0.0702 | 0.0535 |
| 1 2 3 4 | 835 772 | 835 747 | 711 703 688 | 790 713 694 | 1,422 628 | 1,422 628 722 | 1,520 1,425 | 1,660 1,585 920 |
| 5 6 7 | 710 708 702 | 705 700 702 | 688 679 686 | 688 679 686 | 710 700 707 | 682 696 | 694 690 | 710 696 |
| 8 9 10 | | | 567 | 567 | | | | |
| 11 12 13 14 15 16 | 571 650 686 702 710 708 | 571 662 690 702 710 713 | 645 675 694 699 | 650 675 689 699 696 | 571 667 690 702 710 708 | 577 678 696 702 710 708 | 571 667 686 689 699 696 | 577 682 690 696 699 7 03 |
| 16 17 18 19 20 21 | 718 732 | 723 722 | 702 684 | 702 701 | 718 722 | 723 726 | 707 910 | 723 1,162 |
| 21 22 23 24 25 | 702 690 672 | 702 690 672 | 680 675 665 | 680 630 672 | 708 701 688 | 708 696 688 | 690 686 679 | 1,580 690 688 |
| 26 27 28 29 | 689 697 762 | 695 697 754 | 673 665 733 | 674 675 733 | 695 697 762 | 701 702 762 | 680 686 749 | 689 697 754 |
| 30 | 710 | 710 | 688 | 688 | 710 | 710 | 716 | 750 |

(e) Test B-1810

| Coolant nozzle | |
|---|-------|
| Туре | |
| Diameter, in | 0.150 |
| Temperature of coolant, OR | 510 |
| Total temperature of free stream, OR | 1,440 |
| Static pressure of free stream, lb/sq in. abs | 14.67 |
| Total pressure of free stream, lb/sq in. abs | 120.4 |
| α , deg α , | 0 |
| Model surface pressure, lb/sq in. abs, at - | |
| Orifice 1 | 55.7 |
| Orifice 2 | 51.7 |
| Orifice 3 | 53.4 |
| Orifice 4 | 50.7 |
| Orifice 5 | |
| Orifice 6 | 57.6 |
| Orifice 7 | 55.7 |
| Orifice 8 | 60.9 |
| 0111100 0 | 50.7 |

| Thermocouple | | Te | mperatur coolant | e on coo flow rat | led wall e, lb/se | , ^O R, fo | r | |
|----------------------------------|--|--|---------------------------------|--|--|--|--|--|
| Thermocoupie | 0.0694 | 0.0645 | 0.0597 | 0.0506 | 0.0431 | 0.0416 | 0.0299 | 0.0183 |
| 1 2 | 680 667 | 695 681 | 690 669 | 768 724 | 756 724 | 805 768 | 1,200 1,150 | 1,170 1,132 |
| 3 4 5 6 | 667 667 651 653 | 670 678 665 | 667 667 | 678 678 665 | 670 670 663 660 | 678 678 665 | 728 688 | 800 765 840 668 |
| 7 8 9 | | | | | | | | |
| 10 11 12 13 14 15 | 558 617 643 656 665 668 | 571 640 663 663 669 672 | 558 625 647 656 666 | 571 645 663 668 678 672 | 567 640 656 656 666 668 | 571 660 667 668 677 672 | 582 667 677 672 677 679 | 588 667 670 668 681 720 |
| 17 18 19 | 660 665 | 673 679 | 668 668 | 673 695 | 674 710 | 680 732 | 740 | 812 |
| 20 21 22 | 651 | 668 | 651 | 668 | 657 | 673 | 673 | 668 |
| 23 24 25 26 27 28 | 655 657 653 654 650 | 666 672 679 675 667 | 661 657 647 654 656 | 669 672 684 669 667 | 666 665 683 660 656 | 675 678 678 716 669 667 | 675 683 738 686 681 | 686 704 885 750 693 |
| 29 30 | 665 | 665 | 665 | 660 | 668 | 668 | 675 | 675 |

(f) Test B-1811

| Coolant nozzle | |
|---|---------------|
| Туре | Axial |
| Diameter, in | 0.150 |
| Temperature of coolant, OR | 510 |
| Total temperature of free stream, OR | 2,000 |
| Static pressure of free stream, lb/sq in. abs | 14.70 |
| Total pressure of free stream, lb/sq in. abs | 120.0 |
| α, deg | 0 |
| Model surface pressure, lb/sq in. abs, at - | |
| Orifice 1 | 56.9 |
| Orifice 2 | 5 0. 2 |
| Orifice 3 | 51.7 |
| Orifice 4 | 49.0 |
| Orifice 5 | |
| Orifice 6 | 57.4 |
| Orifice 7 | 54.5 |
| Orifice 8 | 59.3 |
| | |

| Thermocouple | | Te | | | oled wall ce, lb/se | | r | |
|--|--|---|---|--|--|--|---|--|
| Thermocoupie | 0.1450 | 0.1332 | 0.1221 | 0.1142 | 0.1130 | 0.1012 | 0.0924 | 0.0666 |
| 1 2 | 702 697 | 723 703 | 756 746 | 745 724 | 1,154 735 | 1,130 741 | 863 1,139 | 1,565 1,350 |
| 3 4 5 6 7 8 | 688 688 679 680 | 694 694 684 685 | 710 705 689 696 | 694 694 684 690 | 705 705 689 696 | 710 705 689 690 | 700 700 689 690 | 705 700 684 696 |
| 9 | | | | | | | | |
| 10 11 12 13 14 15 16 17 18 | 567 656 696 696 704 702 | 571 656 696 696 704 702 711 | 587 705 702 696 710 702 718 | 588 657 696 696 704 702 | 583 705 703 703 715 708 | 583 671 702 702 710 702 | 592 678 711 708 .715 709 | 693 688 718 708 715 708 |
| 1 [.] 9 20 | 695 | 701 | 710 | 710 | 717 | 717 | 971 | 1,193 |
| 21 22 | 679 | 685 | 697 | 685 | 697 | 697 | 690 | 690 |
| 23 24 25 26 27 28 | 685 683 679 680 677 | 685 683 679 680 681 | 690 693 701 697 691 | 685 683 679 680 681 | 696 693 695 691 691 | 690 693 695 691 691 | 696 694 694 691 686 | 696 693 726 691 691 |
| 29 30 | 697 | 697 | 697 . | 697 | 697 | 686 | 697 | 686 |

(g) Test B-1813

| Coolant nozzle | |
|--|---------|
| Type | xial |
| 2100010 001 1 1 1 1 1 1 1 1 1 1 1 1 1 1 | .150 |
| Tomporturate of Coofficient, in the Confession of the Confession o | 510 |
| 10 tol toll polarisa of 2 tol toll toll toll toll toll toll tol | ,500 |
| 504010 probbate 01 1100 Bulletin, 1-/1-1 | 4.53 |
| 10 dai pressare of free boream, 15/54 in and 1 to 1 to 1 to 1 to 1 | 19.2 |
| α, deg | 0 |
| Model surface pressure, lb/sq in. abs, at - | |
| Orifice 1 | |
| Orlice 2 | |
| | 50.2 |
| Office + | 47.7 |
| Orifice 5 | |
| Office of a second of the contract of the cont | |
| Orifice 7 | 52.1 |
| Orifice 8 | |

| Thermocouple | | Te | mperatur coolant | e on coo flow rat | led wall e, lb/se | , ^O R, fo | r | |
|---------------------------------------|--|--|--|---------------------------------|--|--|--|--|
| The Timo Coupie | 0.1578 | 0.1487 | 0.1418 | 0.1320 | 0.1140 | 0.1118 | 0.0959 | 0.0771 |
| 1 2 | 825 781 | 726 684 | 862 807. | 799 754 | 973 798 | 88o | 1,568 935 | 1,740 1,540 |
| 3 4 5 6 | 731 736 | 68 0 698 | 725 742 | 680 709 | 680 709 | 725 725 | 720 709 | 788 725 |
| 7 8 | 714 | 693 | 714 | 688 | 671 | 714 | 704 | 709 |
| 9 10 11 12 13 14 15 | 577 653 687 699 712 712 | 569 653 678 684 708 701 | 577 665 697 710 723 712 | 659 687 699 708 701 | 569 669 691 699 708 706 | 574 669 697 709 712 712 | 569 674 697 699 708 706 | 578 690 707 710 712 712 |
| 17 18 19 20 | 721 | 705 709 | 731 | 709 724 | 691 751 | 712 | 715 794 | 709 |
| 21 22 23 24 25 | 711 698 701 | 694 692 695 | 740 703 701 | 701 698 701 | 707 698 701 | 720 703 705 | 711 709 705 | 718 709 711 |
| 26 27 28 | 709 | 694 | 714 | 694 | 699 | 709 | 70 ¹ 4 | 709 |
| 29 30 | 627 | 616 | 623 | 616 | 610 | 616 | 602 | 688 |

(h) Test B-1814

| Type | |
|---|----|
| | 50 |
| Diameter, in | |
| Temperature of coolant, OR | - |
| Total temperature of free stream, OR | |
| Static pressure of free stream, lb/sq in. abs 14. | |
| Total pressure of free stream, lb/sq in. abs | |
| a, deg | 5 |
| Model surface pressure, lb/sq in. abs, at - | |
| Orifice 1 | |
| Orifice 2 | |
| Orifice 3 | _ |
| Orifice 4 42 | - |
| Orifice 5 | |
| Orifice 6 | |
| Orifice 7 | •9 |
| Orifice 8 | |

| Thermocouple | | Temper cool | rature on Lant flow | cooled wa | ll, ^O R, f | for | |
|---|--|--|--|--|--|--|--|
| | 0.0771 | 0 .0 652 | 0.0 592 | 0.0571 | 0.0520 | 0.0 488 | 0.0387 |
| 1 2 3 | 1,510 | 1,031 | 1,510 | 1,170 | 1,425 | 1,290 | 1,435 |
| 4 5 6 | 1,425 | 792 724 | 1,450 | 1,096 914 | 1,410 | 1,260 | 1,445 |
| 7 8 | 709 | 667 | 778 | 709 | 800 | 866 | 1,345 |
| 9 10 11 12 13 14 15 16 17 | 568 673 691 695 701 717 | 552 642 653 660 667 681 | 573 684 691 695 734 891 | 559 658 664 679 689 759 | 573 679 681 688 817 1,215 | 569 673 671 701 811 1,044 | 589 722 873 1,179 1,315 1,350 |
| 19 20 21 22 | 682 | 891 990 643 | 687 | 1,082 1,125 654 | 677 | 666 | 681 |
| 23 24 25 26 | 712 769 | 681 709 | 875 1,270 | 775 805 | 1,255 1,360 | 1,108 1,202 | 1,398 1,440 |
| 27 28 | 834 | 743 | 1,378 | 865 | 1,385 | 1,220 | 1,432 |
| 29 30 | 862 | 643 | 693 | 660 | 681 | 670 | 681 |

TABLE I.- BASIC DATA - Continued

(i) Test B-1815

| Coolant no: | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|----------------|-----|----|-----|-----|----|-----|-----|-----|-----|----|-----|-----|----|-----|-----|-----|----|---|---|---|---|---|---|---|---|---|---|---|---|---|--------------|
| Type | | | | | | | | | | | | | | | | | | | • | | | | | | • | • | ٠ | | | • | Umbrella |
| Clearance | e, | ir | ١. | | | | | | | | | | | | | | | | | | | | | ٠ | • | | | | • | • | 0.0025 |
| Temperature | e o | ſ | cc | ool | ar | ıt, | , (| PR | | | | | | | | | | | | | | | | | | • | | | • | • | 510 |
| Total tempe | era | tυ | ıre | • (|)f | fı | ·ee | 9 5 | tr | e٤ | ım, | , (| R | | | | | ٠ | | • | | | | | • | | | | • | • | |
| Static pres | ssu | re | 3 (|)f | fı | ree | 9 8 | str | ee | m, | , 1 | Lb, | so | 1 : | in. | . ε | bs | 3 | | • | | | • | • | • | ٠ | | | • | | 14.57 |
| Total press | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 120.4 |
| α , deg | | | | | | • | | | . • | | | | | | • | • | • | • | • | | • | • | | • | • | • | • | | ٠ | • | 5 |
| Model surfa | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Orifice : | 1 | | | | | | | ٠ | | | • | | • | • | • | • | ٠ | | • | ٠ | ٠ | ٠ | • | ٠ | • | ٠ | • | • | ٠ | ٠ | |
| Orifice : | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 10.0 |
| Orifice | | | | | | | | | | | | | | | • | | | | | | | | | | | | | | | | 48.8 |
| Orifice | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 3 5.1 |
| Orifice | 5 | • | | | • | | | • | | • | • | | • | • | • | | • | • | • | ٠ | • | • | ٠ | ٠ | ٠ | ٠ | ٠ | ٠ | ٠ | ٠ | |
| Orifice (| 6 | | | | | | | | ٠ | | • | | | • | • | • | | • | ٠ | ٠ | • | • | • | • | • | • | ٠ | • | ٠ | • | |
| Orifice ' | 7 | | | | | ٠ | | | | | | | | • | | | | • | | ٠ | • | • | ٠ | • | • | • | ٠ | | • | ٠ | 50.0 |
| Orifice (| 3 | ٠ | ٠ | • | • | | | | | • | • | • | • | • | • | ٠ | • | ٠ | ٠ | • | • | ٠ | ٠ | • | ٠ | • | ٠ | ٠ | • | • | |

| Thermocouple | | Te | mperatur coolant | e on coo flow rat | led wall e, lb/se | , ^O R, fo | r | |
|---|--|--|--|--|--|--|--|--|
| Thermocouple | 0.0840 | 0.0735 | 0.0722 | 0.0596 | 0.0500 | 0.0416 | 0.0250 | 0.0167 |
| 1 2 3 4 | 829 735 | 1,270 | 1,083 | 1,305 768 | 1,305 | 1,287 | 1,310 768 | 1,313 746 |
| 5 6 7 8 | 650 | 970 | 651 | 862 | | 1,288 | 1,318 | 1,318 |
| 9 10 11 12 13 14 15 16 | 533 615 643 653 656 652 | 538 626 658 666 684 710 | 538 630 647 653 656 670 | 553 652 663 670 745 804 | 568 717 916 1,285 1,320 1,318 | 593 1,044 1,163 1,285 1,320 1,318 | 660 1,197 1,249 1,305 1,320 1,318 | 735 1,238 1,279 1,305 1,333 1,323 |
| 17 18 19 20 21 22 | 703 769 615 | 1,196 1,223 | 768 1,029 | 1,080 1,083 | 1,313 1,275 | 1,313 1,274 | 1,313 1,295 | 1,319 1,311 631 |
| 23 24 25 26 27 | 663 | 723 866 | 687 744 | 1,153 1,325 | 1,318 1,330 | 1,318 1,325 | 1,335 1,345 | 1,345 1,350 |
| 28 29 30 | 671 586 | 1,247 597 | 774 711 | 1,320 578 | 1,320 578 | 1,320 637 | 1,332 | 1,320 898 |

(j) Test B-1816

| Coolant nozz | le | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|---|-----------|-----|-----|--------------|-----|-----|------|--------|----|--------|-----|-----|-----|-----|-----|-------------|---|---|---|---|-------|---|---|-------|---|---|---|---|--------------|
| Туре | | | | | | | | | | | | | | | | | | | | | | | | | | | | | Axial |
| Diameter, | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 0.050 |
| Temperature | $\circ f$ | c | oc. | Lar | ıt, | , (| PR | | | | | | | | | | | | | | | | | | | | | | None |
| Total temper | atı | ure | e (| \mathbf{f} | fr | •ee | 9 8 | tr | ea | m, | , с | R | | | | | | | | | | | | | | | | | 1,360 |
| Static press | ure | e d | οſ | fı | ee | 9 8 | tr | ea | m, | . 1 | .b/ | sq. | ı i | ln. | , ε | bs | 3 | | | | | | | | | | | | 14.80 |
| Total pressu | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 120.5 |
| α , deg | | | | | | | | | | | | | | | | | | | | | | | | | | • | | • | 0 |
| Model surfac | _ , | | | * 1 1 2 | 10 | 1 | 1. / | | | ~ | | ha | | 0.4 | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Orifice l | | pre | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Orifice l Orifice 2 | | | | | • | | • | | | | | | | | | | | | | | | | | | | | | | |
| Orifice 1 Orifice 2 Orifice 3 | • | | | | • | : | • | : | | | | | • | : | : | : | • | | | | | | | | | | | | 53.5 |
| Orifice 1 Orifice 2 Orifice 3 Orifice 4 | : | | • | · · | | • | • | · · | • | · · | : | : | • | : | : | : | | : | | : | : | : | : | : | • | | : | | |
| Orifice 1 Orifice 2 Orifice 3 Orifice 4 Orifice 5 | | | : | | | | | : | | • | | | | | | · · · | : | | : | | | | | | | | | | 53.5 |
| Orifice 1 Orifice 2 Orifice 3 Orifice 4 Orifice 5 Orifice 6 | | | | | | | | | | • | | | | | | : | | : | | | • | : | | : | : | | | | 53.5 51.3 |
| Orifice 1 Orifice 2 Orifice 3 Orifice 4 Orifice 5 | | | | | | | | | | • | | | | | | : | : | : | | | | : | | : | : | | | | 53.5 51.3 |

| Thermocouple | | ı | Transien | | atures or | | ^o R, | |
|---|---------|---|--|--|-----------|--|--|---|
| - | 0.5 | 1.5 | 2.5 | 3.5 | 4.5 | 7.5 | 10.5 | 16.5 |
| 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24 25 | 690 | 875 893 908 721 908 907 880 910 900 878 835 902 902 | 786 1,024 786 1,026 1,021 984 1,031 1,011 958 1,019 | 1,070 1,083 1,102 1,102 828 1,099 1,097 1,092 1,070 1,026 1,097 1,099 | 1,116 | 1,204 1,218 1,213 1,213 1,213 1,168 1,232 1,217 1,207 1,162 1,211 1,231 | 1,237 1,252 1,241 1,240 1,238 1,186 1,253 1,241 1,236 1,235 | 1,254 1,262 1,258 1,258 1,257 1,254 1,198 1,267 1,252 1,248 1,248 |
| 26 27 | | 902 | 1,029 | 1,110 | 1,155 | 1,235 | 1,255 | 1,264 |
| 28 29 30 | 699 | 898 | 1,010 | 1,091 | 1,140 | 1,221 | 1,252 | 1,265 |

TABLE I.- BASIC DATA - Concluded

(k) Test B-1818

| Coolant nozzle Type | |
|--|----|
| Temperature of coolant, OR | LO |
| Total temperature of free stream, OR | 50 |
| Static pressure of free stream, lb/sq in. abs $\dots \dots 14.5$ | - |
| Total pressure of free stream, lb/sq in. abs | .7 |
| a, deg | 0 |
| Model surface pressure, lb/sq in. abs, at - | |
| Orifice 1 | |
| Orifice 2 | |
| Orifice 3 | |
| Orifice 4 | .6 |
| Orifice 5 | |
| Orifice 6 | |
| Orifice 7 | .6 |
| Orifice 8 | |

| Thermocouple | | Te | mperatur coolant | e on coo flow rat | led wall ce, lb/se | oR, fo | or | |
|----------------------|--------------------------|---------------------------------|--------------------------|--------------------------|--------------------------|--------------------------|--------------------------|--------------------------|
| The Imocoupte | 0.2140 | 0.1970 | 0.1913 | 0.1844 | 0.1790 | 0.1705 | 0.1614 | 0.1490 |
| 1 2 | 723 | 735 | 830 | 830 | 790 | 830 | 832 | 880 |
| 3 4 5 | 710 | 720 | 733 | 738 | 721 | 738 | 718 | 738 |
| 5 6 7 8 | 695 | 706 | 733 | 727 | 710 | 727 | 719 | 733 |
| 9 10 | | | 610 | 599 | 567 | 586 | 576 | 576 |
| 11 12 13 14 | 570 650 681 900 | 570 661 687 705 713 | 670 702 716 725 | 670 702 710 713 | 655 697 711 720 | 678 706 717 720 | 678 707 717 725 | 682 710 722 731 |
| 15 16 17 18 | 713 712 711 | 719 718 | 724 734 | 719 | 719 722 | 719 728 | 724 728 | 730 734 |
| 19 20 21 | 717 | 749 | | | 780 | | | |
| 22 | | | | | | | | |
| 23 24 25 26 | 694 694 | 704 704 | 713 720 | 720 710 | 713 705 | 720 720 | 720 710 | 720 713 |
| 27 28 | 678 | 703 | 728 | 728 | 712 | 723 | 723 | 728 |
| 29 30 | 624 | 531 | 536 | 531 | 531 | 616 | 531 | 531 |

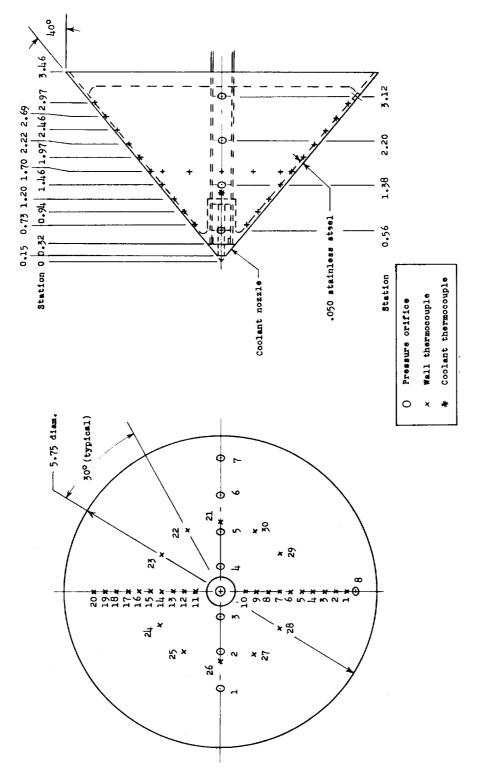
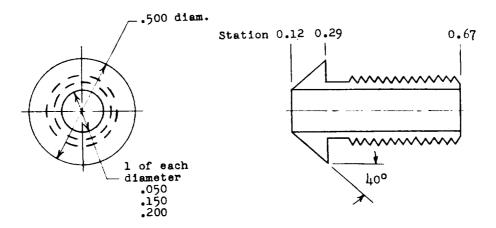


Figure 1.- Drawing of 80° total-angle cone showing locations of thermocouples and pressure orifices. All dimensions are in inches.



Axial nozzles

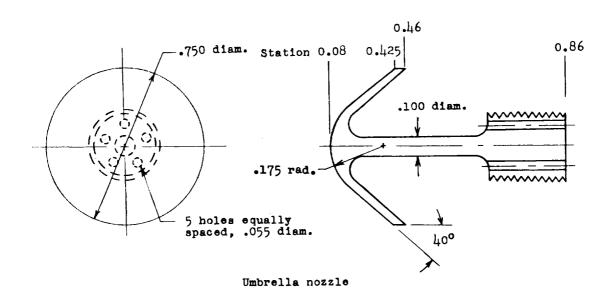


Figure 2.- Drawings of the four nozzles (not to scale). All dimensions are in inches.



Figure 3.- Photograph of the 80° total-angle cone mounted in the ethylene-heated high-temperature jet.

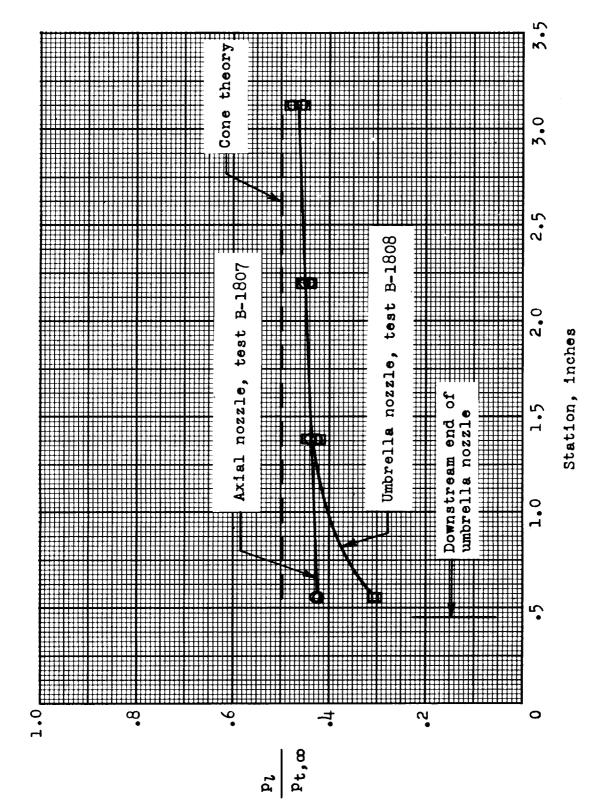


Figure h.- Typical pressure distributions for the two types of coclant flow nozzles.

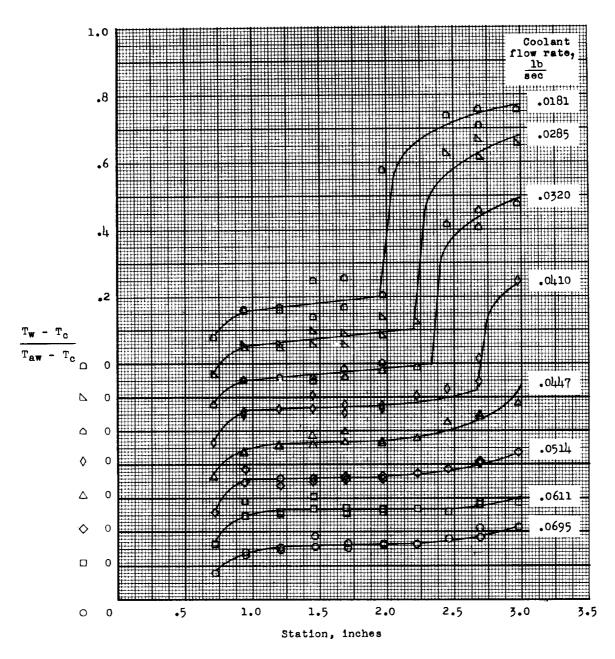


Figure 5.- Temperature distributions for a series of coolant flow rates from a typical test (test B-1807).

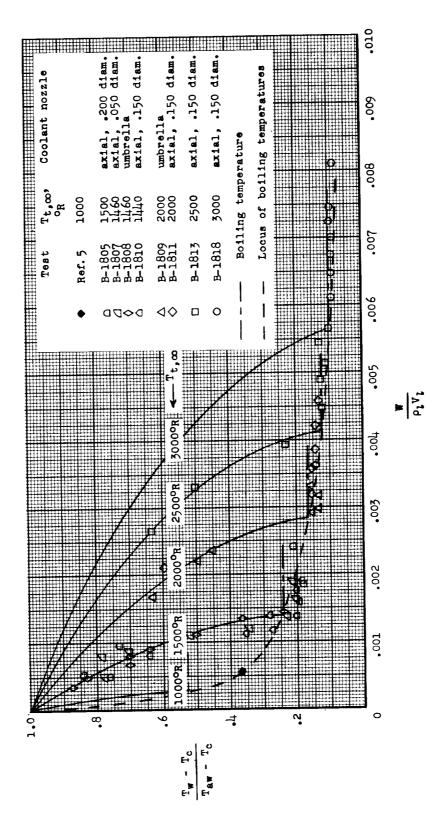


Figure 6.- Effect of flow rate parameter on the temperatures at the thermocouple station farthest downstream.

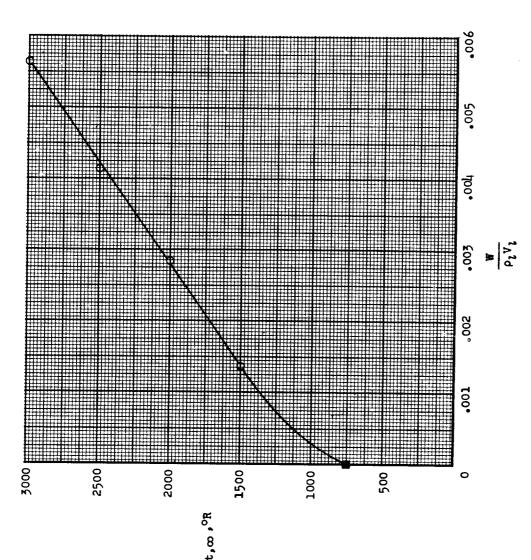


Figure 7.- Minimum flow rates necessary to maintain boiling temperature of coolant (approximately 750° R for this model) at thermocouple station farthest downstream as a function of freestream total temperature.

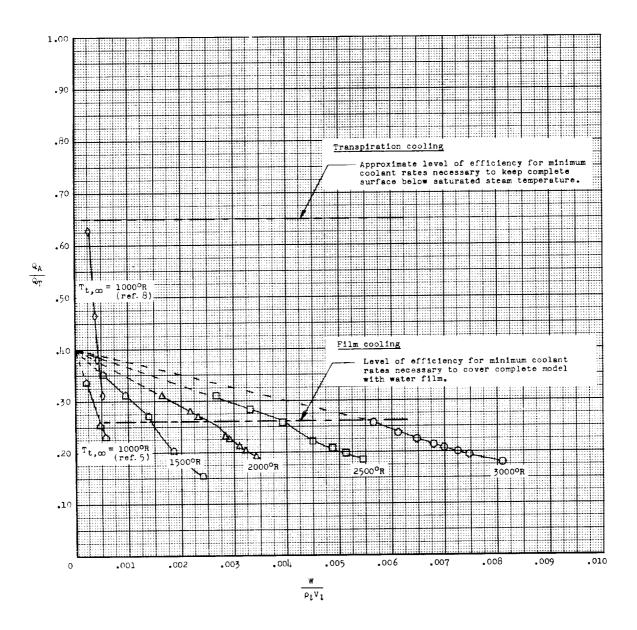
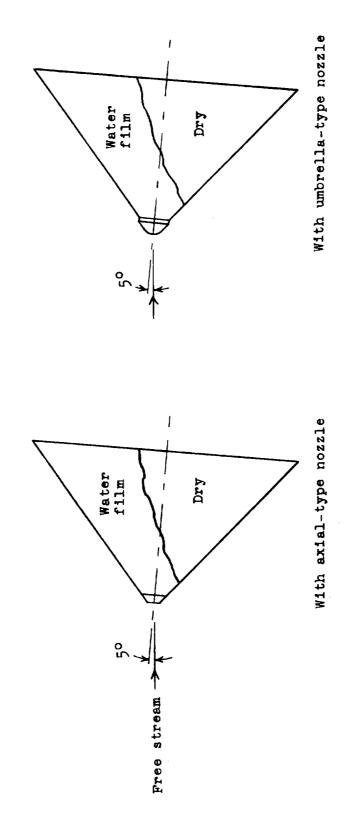


Figure 8.- Efficiency of film cooling from reference 5 and present tests, and of transpiration cooling from reference 8.



for $\alpha = 5^{\circ}$ Figure 9.- Sketch showing approximately the water film asymmetry at each type of coolant nozzle.

| NASA MEMO 12-27-58L National Aeronautics and Space Administration. WATER-FILM COOLING OF AN 80° TOTAL- ANGLE CONE AT A MACH NUMBER OF 2 FOR AIRSTREAM TOTAL TEMPERATURES UP TO 3,000° R. Howard S. Carter. January 1959. 32p. diagrs., photo., tab. (NASA MEMORANDUM 12-27-58L) (Film-cooling tests, with water as the coolant, were made on an 80° total-angle cone in a Mach number 2 free jct at sea-level pressure. The tests were made at free-stream total temperatures from 1,500° to 3,000° R and at free-stream Reynolds numbers per foot from 8 x 10° to 3 x 10°. With low coolant rates, the downstream end of the model became very hot. Increasing the angle of attack from 0° to 5° caused the water film on the model surface to become very | 1. Heat Transfer, Aerodynamic (1.1.4.2) 2. Bodies - Surface Conditions (1.3.2.4) I. Carter, Howard S. II. NASA MEMO 12-27-58L | NASA MEMO 12-27-58L National Aeronautics and Space Administration. WATER-FILM COOLING OF AN 80° TOTAL- ANGLE CONE AT A MACH NUMBER OF 2 FOR AIRSTREAM TOTAL TEMPERATURES UP TO 3,000° R. Howard S. Carter. January 1959. 32p. diagrs., photo., tab. (NASA MEMORANDUM 12-27-58L) (Title, Unclassified) Film-cooling tests, with water as the coolant, were made on an 80° total-angle cone in a Mach number 2 free jet at sea-level pressure. The tests were made at free-stream total temperatures from 1,50° to 3,000° R and at free-stream Reynolds numbers per foot from 8 x 10° to 3 x 10°. With low coolant rates, the downstream end of the model became very hot. Increasing the angle of attack from 0° to 5° caused the water film on the model surface to become very | 1. Heat Transfer, Aerodynamic (1.1.4.2) 2. Bodies - Surface Conditions (1.3.2.4) I. Carter, Howard S. II. NASA MEMO 12-27-58L |
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| NASA MEMO 12-27-58L National Aeronautics and Space Administration. WATER-FILM COOLING OF AN 80° TOTAL- ANGLE CONE AT A MACH NUMBER OF 2 FOR AIRSTREAM TOTAL TEMPERATURES UP TO 3,000° R. Howard S. Carter. January 1959. 32p. diagrs., photo,, tab. (NASA MEMORANDUM 12-27-58L) Film-cooling tests, with water as the coolant, were made on an 80° total-angle cone in a Mach number 2 free jet at sea-level pressure. The tests were made af free-stream total temperatures from 1,500° to 3,000° R and af free-stream Reynolds numbers per foot from 8 x 106 to 3 x 106. With low coolant rates, the downstream end of the model became very hot. Increasing the angle of attack from 0° to 5° caused the water film on the model surface to become very asymmetrical. | 1. Heat Transfer, Aerodynamic (1.1.4.2) 2. Bodies - Surface Conditions (1.3.2.4) I. Carter, Howard S. II. NASA MEMO 12-27-58L | NASA MEMO 12-27-58L National Aeronautics and Space Administration. WATER-FILM COOLING OF AN 80° TOTAL- ANGLE CONE AT A MACH NUMBER OF 2 FOR AIRSTREAM TOTAL TEMPERATURES UP TO 3,000° R. HOWARD S. Carter. January 1959. 32p. diagrs., photo., tab. (Title, Unclassified) Film-cooling tests, with water as the coolant, were made on an 80° total-angle cone in a Mach number 2 free jet at sea-level pressure. The tests were made at free-stream total temperatures from 1,500° to 3,000° R and at free-stream Reynolds numbers per foot from 8 x 10° to 3 x 10°. With low coolant rates, the downstream end of the model became very hot. Increasing the angle of attack from 0° to 5° caused the water film on the model surface to become very asymmetrical. | 1. Heat Transfer, Aerodynamic (1.1.4.2) 2. Bodies - Surface Conditions (1.3.2.4) I. Carter, Howard S. II. NASA MEMO 12-27-581. |
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